APPENDIX I

SPECIFICATION AMENDMENTS:

Amend the specification of the application as set forth the following:

Page 11, lines 7-14, please rewrite the paragraph as follows:

50 kg steatite (magnesium silicate)-rings haing an outer diameter of 8 mm, a length of 6 mm and a wall thickness of ~~1,5~~1.5 mm were heated to 160 °C in a coating pan and spray-coated with a supsension of ~~28,6~~28.6 kg anatase having a BET surface of 20 m^2/g, ~~2,19~~2.19 kg vanadyl oxalate, ~~0,176~~0.176 kg cesium sulphate, ~~44,1~~ 44.1 kg water and ~~9,14~~9.14 kg formamide until the weight of the applied coating yielded ~~10,5%~~10.5% of the total weight of the catalyst (after calcination at 450 °C).

Page 11, lines 15-18, please rewrite the paragraph as follows:

The catalytic coating thus applied, i.e. the catalyst shell, consisted of ~~4,0~~ 4.0 percent by weight vanadium (calculated as V_2O_5), ~~0,4~~ 0.4 percent by weight cesium (calculated as Cs) and ~~95,6~~ 95.6 percent by weight titanium dioxide.

Page 11, lines 21-29, please rewrite the paragraph as follows:

50 kg steatite (magnesium silicate) –rings having an outer diameter of 8 mm, a length of 6 mm and a wall thickness of ~~1,5~~1.5 mm were heated to 160 °C in a coating pan and spray-coated with a suspension of ~~28,6~~28.6 kg anatase having a BET surface of 20 m^2/g, ~~4,11~~ 4.11 kg vanadyl oxalate, ~~1,03~~1.03 kg antimony trioxide, ~~0,179~~0.179 kg ammonium dihydrogenphosphate, ~~0,045~~0.045 kg cesium sulphate, ~~44,1~~ 44.1 kg water and ~~9,14~~9.14 kg formamide until the weight of the applied coating yielded ~~10,5%~~10.5% of the total weight of the catalyst (after calcination at 450 °C).

Page 11, lines 30-35, please rewrite the paragraph as follows:

The catalytic coating thus applied, i.e. the catalyst shell, consisted of ~~0,15~~0.15 percent by weight phosphorus (calculated as P), ~~7,5~~7.5 percent vanadium (calculated as V_2O_5),

~~3,2~~3.2 percent by weight antimony (calculated as Sb_2O_3), ~~0,1~~ 0.1 percent by weight cesium (calculated as Cs) and ~~89,05~~89.05 percent by weight titanium dioxide.

Page 11, lines 40-47, page 12, lines 1-5, please rewrite the paragraph as follows:

A tube bundle having an external diameter of d_{RBa} = 5.435 m was located in the reactor of the present invention. The tube bundle consisted of about 14,000 catalyst tubes made of steel which each had a length of 3.5 m and an external diameter d_a was thus 1.3793. 4 standard m^3/h of air having a loading of 98.5% purity by weight o-xylene of 90 g/standard m^3 were passed through the tube from the top downward. The ~~etalyst~~ catalyst tubes were filled in a manner to provide for two catalyst zones with different activity. Firstly, catalyst II was filled into each tube to a total height of (as measured from the bottom of the tubes) of ~~1,3~~1.3 m. Then a total ~~1,7~~1.7 m catalyst I was filled into each tube on top of the catalyst II layer.

Page 4, first paragraph, line 2, please rewrite the paragraph as follows:

We have found that this object is achieved by the multitube reactor ~~having the features of claim 12~~ as described herein. According to the present invention, it is proposed that in the case of relatively large reactors in which a large amount of heat of reaction is generated owing to the numerous catalyst tubes and has to be removed, the ratio of tube spacing *t* to external tube diameter d_a be made dependent on the reactor diameter or on the external tube bundle diameter d_{RBa}. In particular, the present invention proposes providing a ratio of tube spacing *t* to external tube diameter d_a of at least 1.3. Preferably, the catalyst tubes are arranged such that three adjacent tubes form a triangle, preferably a equilateral triangle. In this case, tube spacing *t* is equal to the length of the sides of the triangle.